

Introduction

Wastewater treatment is an expensive proposition for many businesses, often the most cost effective solution is to ship all waste offsite for treatment. The most energy-intensive portion of the treatment process is aerating the wastewater to facilitate microbial oxidation of organic compounds. Microbial Fuel Cells have been immerging in recent years as an energy-saving substitute for wastewater aeration. We have partnered with a local winery in Santa Rosa and have deployed a pilot system that combines anaerobic digestion (AD) with microbial fuel cell (MFC) technology for the treatment of wine waste onsite. Results gathered from the testing and optimization of this system will inform the development of full-scale AD-MFC-based systems to treat winery wastewater to a level suitable for irrigation while producing energy.

Methods

AD-MFC (Anaerobic Digester Microbial Fuel Cell): A 50-liter custom acrylic cylinder was used as our digester. The cylinder contained a rubber spiral in order to create a channel the waste must follow to ensure maximum retention time. The waste was fed into the cylinder by a peristaltic pump at 8.8 ml/min. This produced a retention time of around 5 days. The electrodes were made of carbon fiber for its corrosion resistant and conductive properties. The anodes were placed one in each quadrant horizontally across the entire cylinder. The anodes were constructed like a bristle brush in order to achieve maximum surface area. There was also a hollow chamber horizontally through the entire cylinder which had walls made of impermeable carbon fiber which was used as a cathode.

Waste: We used wine waste from a local winery to feed the MFC. The waste was stored in a 350 gal "pH stabilization tank" from which our pump could draw feed directly. Due to the acidic nature of the waste (around 3.5pH) we would dilute the waste at a ratio of 1L of waste to 5L of water. If the pH in the feed tank dropped below 6.8, potassium carbonate was added to neutralize the acid and buffer the solution.

Data collection: Voltage was tracked using an off the shelf voltage logger. The logger collected an instantaneous voltage reading each hour. We had a unique device that would open the circuit and allow voltage potential to build up.

COD Removal (Chemical Oxygen Demand) was tracked using mail order kits. Samples were collected directly from the effluent and influent lines. The difference in the COD readings determines the COD removal. Samples were analyzed in a spectrometer for absorbance at 600 nm and compared to known standards. Both soluble and total COD removal were calculated. Total COD removal was determined using unmodified samples. Soluble COD was determined by centrifuging both influent and effluent samples for 5 min at 2000 *g*.

Daily data pH and temperature data were collected via a Mettler-Toledo GmbH handheld probe.

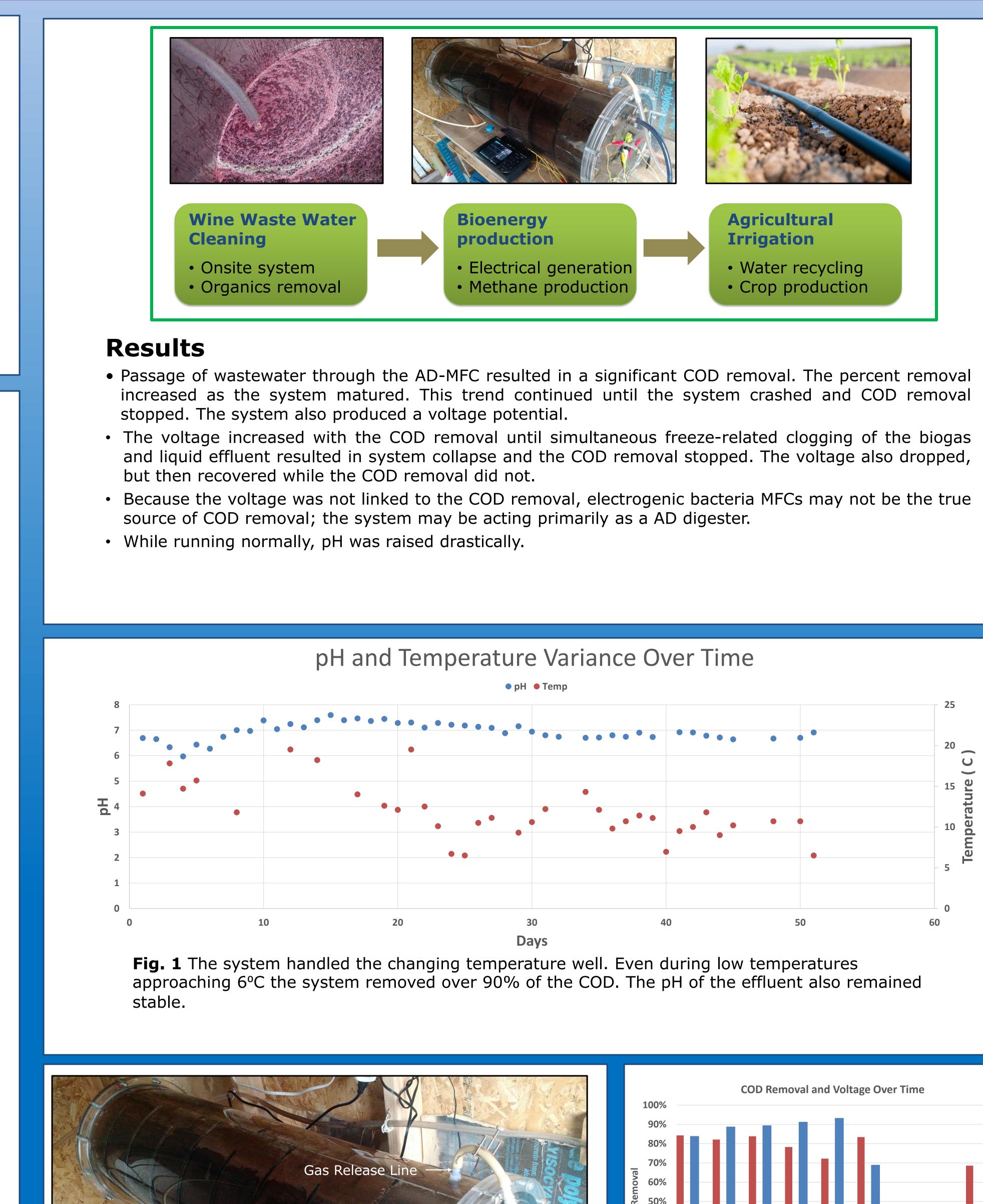
The gas sample was analyzed by a local lab (Analytical Science in Petaluma, CA.) via gas chromatography. The gas was gathered by feeding our gas escape line directly into a gas sample collection bag.



Image 2 The field site located at Vintners Square in Santa Rosa, CA. No significant data was gathered from the Aquatic Scrubber

Development of a hybrid anaerobic digestion-microbial fuel cell system for treating winery wastewater

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Carbon Anode Brush

Loaaer **Image 1** The AD-MFC system is a unique 50 liter acrylic.

Acrylic was chosen for the ability to view the internal section of the AD-MFC during field tests.

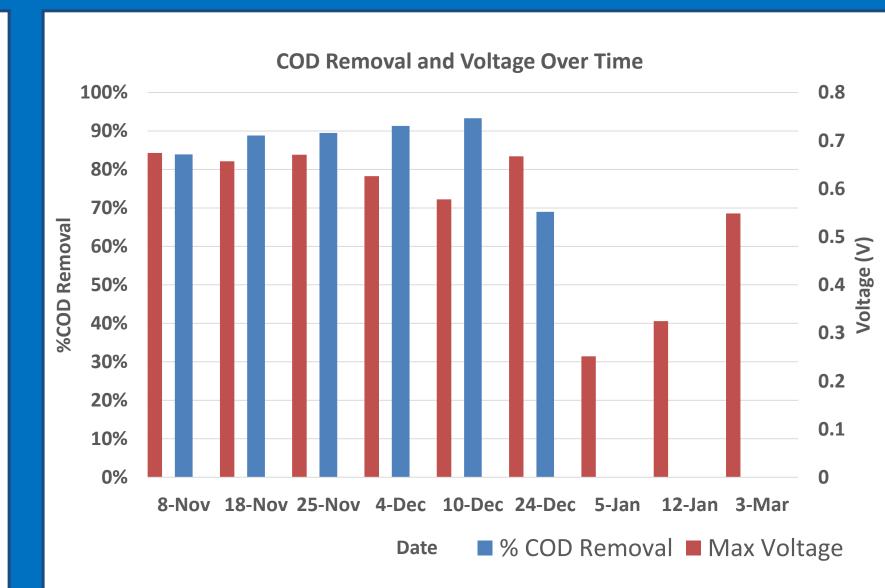


Fig. 2 COD removal gradually increased with time until the system exhibited massive COD removal reduction on the 23rd of Dec. Voltage is not related to our COD removal.

	Change • Pre-Crash pH Ch 1 1 0.5 -0.5 -1
	Amount [mole%]
	- 0.00330
	2.48103
	9.14150
	57.55491
	- 10.42170
•	Conclusion The system scale high-effection at ambient to the pump. Gas producto tubular shap the biogas. The AD-MFC removal. Fur while control The system field applicat Biogas is p standard AD



in pH Each Day

nange 🔹 🗕 Post-Crash pH Change

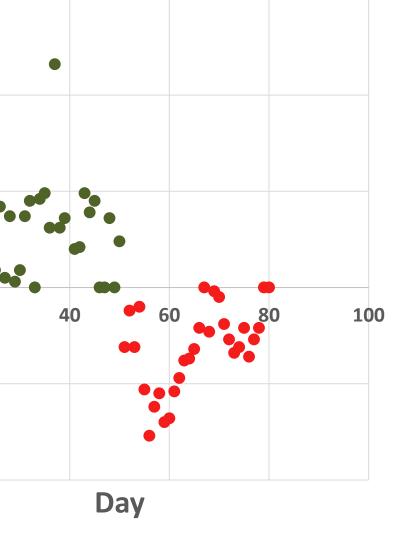


Fig. 3. The AD-MFC increased the pH of the effluent relative to the influent pH during nominal functioning. After the crash the pH was decreased by the AD-MFC. Potentially whatever is removing the COD is also increasing pH.

	Name
	Helium
)	Hydrogen
}	Oxygen
)	Nitrogen
1	Methane
	Carbon Monoxide
)	Carbon Dioxide

Table 1. The gas produced
 by the MFC was mostly methane with significant levels of carbon dioxide. This is consistent with current waste water anaerobic digesters. About 20% of the sample was unaccounted for, possibly because the gas was not detectable by our gas chromatographer. The oxygen and nitrogen is probably due to atmospheric contamination as the ratios are the same as ambient ratios.

ons and Future Prospects

displayed COD removal efficiency close to that of fullefficiency anaerobic digesters. However, our system ran temperatures with the only energy input being that of

ction is similar to that of anaerobic digesters. The be of the enclosed system allows for easy harvesting of

technology may only utilize the AD process for COD rther trials will be needed to compare similar systems lling for electrode presence.

should be able to run with minimal supervision in a tion.

produced with methane concentrations similar to systems.

ledgements

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tend our gratitude to the SOURCE and WATERS their generous grants used to fund student and the development of a field trial.





